- 4 -

RF 128,1282USN 2-Oct-05

In the claims:

Please amend the claims as shown below:

- 1. (Currently amended) A method for dewatering and washing a lime mud (106) before dewatered lime mud is transported to a lime mud kiln, comprising: (200) characterised in that the dewatering of the lime mud takes place in a pressurised pressurized filter (102),
- that the pressurised connecting the pressurized filter (102) is connected to a closed gas circulation system (101), that connecting a filtrate tank (108) is connected to a the filtrate side of the pressurized filter and where a fluid level of filtrate (109) is established from the pressurised
- 15 <u>pressurized</u> filter (102),

 that the pressurised pressurizing the pressurized filter,

 (102) is pressurised in that
 - a compressor $\frac{(111)}{drawing}$ on $\frac{draws}{draws}$ gas phase from the filtrate $tank_{L}$ $\frac{(108)}{draws}$ and $\frac{draws}{draws}$
- pressurized side of the compressor pressurizing, via the gas circulation system, a lime mud side of pressurises the pressurized filter,

 (102) on the pressurised side of the compressor, on the lime mud side of the filter, that a certain
- 25 <u>venting a</u> pre-determined amount of <u>the</u> gas phase <u>is vented</u>
 from the gas circulation system (101),
 and that adding an equivalent pre-determined amount of fresh
 air <u>is added</u> to <u>the</u> a recycled gas phase <u>to</u> with the aim of
 maintaining <u>the</u> a partial pressure of oxygen gas above a predetermined minimum level.
 - 2. (Currently amended) The method according to claim 1,

- 5 -

RF 128.1292USN 2-Oct-06

characterised in that the wherein a temperature in the pressurized pressurised filter (102), including a the temperature of the recycled gas phase, is maintained above 75°C, preferably 75-95°C.

5

10

15

20

- 3. (Currently amended) The method according to either claim 1 or 2, characterised in that the claim 1 wherein an amount of residual white liquor in the lime mud (106) does not exceed 10%, preferably under 5%, of the white liquor that is formed in the a previous causticization step.
- 4. (Currently amended) The method according to any one-of claims 1-3, characterised in that claim 1 wherein the lime mud that has been filtered out from the lime mud is dry-fed out from the a disc filter for onwards transportation to the lime mud kiln (200).
- 5. (Currently amended) The method according to any one of claims 1-4, characterised in that claim 1 wherein de-airing of the recycled gas phase is carried out on the pressurized pressurised side (p) of the compressor via a de-airing device (113a), and in that and an addition of fresh air is carried out by an air-supply device (112a) connected to the suction side (s) of the compressor.

25

30

6. (Currently amended) The method according to any one of claims 1-4, characterised in that claim 1 wherein de-airing of recycled gas phase is carried out on the suction side (s) of the compressor at a first distance from the an inlet to the compressor via a de-airing device (113a), and in that and an addition of fresh air is carried out through an air-supply device (112a) on the suction side (s) of the

RF 128.1282USN 2-Oct-06

15

20

25

30

compressor at a second distance from the an inlet to the compressor, where the first distance is greater than the second distance.

- 7. (Currently amended) The method according to any one of the preceding claims, characterised in that the claim 1 wherein an amount of recirculated gas phase that is exchanged lies within the an interval 5-20%, preferably less than 10%.
- 8. (Currently amended) The method according to any one of the preceding claims, characterised in that the claim 1 wherein an amount of recirculated gas phase that is exchanged is regulated such that it the amount depends on a detected process parameter.
 - 9. (Currently amended) The method according to claim 8, characterised in that wherein the detected process parameter is the partial pressure of oxygen gas in the pressurized filter.
 - 10. (Currently amended) The method according to claim 8, characterised in that wherein the detected process parameter is the a flow rate of flow of lime mud or dewatered lime mud, or parameters that are representative of these flow rates of flow.
 - 11. (Currently amended) The method according to any one of the preceding claims, characterised in that claim 1 wherein the pressurized pressurised filter is of the a disc filter type.

RF 128.1282USN 2-Oct-06

- 12. (Currently amended) An arrangement for washing and dewatering a lime mud before dewatered lime mud is transported to a lime mud kiln, comprising: (200) characterised in that the dewatering of the lime mud takes place in a
- pressurised pressurized filter (102),

 that arranging a recirculation line 110 is arranged for a gas phase from the a filtrate side to the of a mud side,

 that connecting the pressurised pressurized filter (102) is connected to a gas circulation system (101) that is
- essentially closed,

 that connecting a filtrate tank (108) is connected to the

 a filtrate side of the pressurized filter and where a fluid
 level of a filtrate (109) is established from the pressurised

 pressurized filter, (102),
- that pressurizing the pressurised pressurized filter, (102)
 is pressurised in that
 a compressor (111) drawing on its a suction side thereof a
 draws gas phase from the filtrate tank (108) and pressurises
 a pressurized side of the compressor pressurizing, via the gas
 circulation system a lime mud side of the pressurized filter,
 (102) on the pressurised side of the compressor, on the lime
 mud side of the filter,
 - that venting a certain pre-determined amount of gas phase $\frac{i \pi}{2}$ vented from the gas circulation system $\frac{101}{2}$, through \underline{a}
- de-airing devices, (113a) and

 that adding an equivalent pre-determined amount of fresh air

 is added through an air-supply devices (112a) to the a

 recycled gas phase with to maintain a the aim of maintaining
 the partial pressure of oxygen gas above a pre-determined

 minimum level.
 - 13. (Currently amended) The arrangement according to claim 12, characterised in that wherein the de-airing device (112a) is

RF 128.1282USN 2-Oct-06

arranged at a position on the <u>pressurized</u> pressurised side (p) of the compressor, and in that the air-supply device (112a) is arranged at a position on the suction side (s) of the compressor.

5

10

- 14. (Currently amended) The arrangement according to claim 12, characterised in that wherein the de-airing device (113a) is arranged at a position on the suction side (s) of the compressor at a first distance from the compressor (111), and in that the air-supply device (112a) is arranged at a position on the suction side (s) of the compressor at a second distance from the compressor (111), where the first distance is greater than the second distance.
- 15. (Currently amended) The arrangement according to any one of claims 12-14, characterised in that claim 12 wherein a control unit (140) controls the regulator valves (112), (160) for at least one of de-airing and addition of air.

20

- 16. (Currently amended) The arrangement according to claim 15, wherein characterised in that the control unit 140 receives input signals from sensors 150.
- 25 17. (Currently amended) The arrangement according to <u>claim 12</u>

 <u>wherein the pressurized any one of claims 12-16,</u>

 characterised in that the pressurised filter (102) is of <u>a</u>

 the disc filter type.